

the catalyst flowing downwards via gravity, each set of the inner annular baffles directing the catalyst to flow outwards towards the same set of the outer annular baffles and then the set of the outer annular baffles directing the catalyst to flow towards the next set of the inner annular baffles, thereby several sets of the inner annular baffles and the outer annular baffles at different heights cause a zigzag flow of the catalyst in the cylinder;

(1) introducing a steam to the annular steam conduit through the steam introducing conduit,

the steam flowing out from the small holes on the annular steam conduit, passing through the small holes in the outer annular baffles and coming into a countercurrent and cross current contact with the regenerated catalyst,

the steam rapidly replacing the flue gas carried by the regenerated catalyst, the removed gas and the excessive steam being collected under each set of inner annular baffles and entering the degassing pipe through the opening part of the degassing pipe;

(2) discharging the stripped regenerated catalyst from the bottom of the stripper; and

(3) venting the removed flue gas and excessive steam in the degassing pipe from the top of the stripper under the action of steam or air from the horizontal pipe.

2. The process according to claim 1, wherein said regenerated catalyst comes from catalytic conversion process.

3. The process according to claim 2, wherein said catalytic conversion processes are catalytic pyrolysis process, or deep catalytic cracking.

4. 3. The process according to claim 1, wherein the

velocity of the regenerated catalyst entering the stripper tangentially is 10-18 m/s.

5. 4. The process according to claim 1, wherein the residence time of the steam in each contact section consisted of inner annular baffles and outer annular baffles is less than 3 s.

6. 5. The process according to claim 1, wherein the velocity of the regenerated catalyst in the stripper is 0.05-0.3 m/s.